



# Rationally designed dipicolinate-functionalized silica for highly efficient recovery of rare-earth elements from e-waste

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## ABSTRACT

Composition of the immobilized layer plays a crucial role in metal adsorption properties of complexing organo-mineral materials. Ignoring the specific features of chemical reactions on solid surface can lead to a significant deterioration in the target properties of the resulted materials. In this research we demonstrated that rationally designed surface-assembling synthesis of organo-silica with covalently immobilized fragments of dipicolinic acid (DPA) resulted in the adsorbent that is capable quantitatively recover almost all Rare Earth elements (REEs) from multielement solution with  $\text{pH} > 1.7$ . In ten consecutive adsorption/desorption cycles no noticeable loss of its efficiency was found, with a mean value of REEs recovery larger than 97%. The adsorbent has been used to recover REEs from model solutions (22 metal ions in  $0.5 \text{ mol L}^{-1}$  NaCl) and real leaching solution of waste of fluorescent lamps. It was demonstrated that even 3200-fold excess of Fe and Cu ions only slightly reduces REEs recovery. The adsorbent is capable to recover above 80% of all (except La) REEs from acidic leaching solution from fluorescent lamps with enrichment factors above 600. After adsorption of  $\text{Eu}^{3+}$  and  $\text{Tb}^{3+}$ , the resulting materials exhibited strong red and green luminescence, respectively, indicating chelating mechanism of REEs adsorption on  $\text{SiO}_2$ -DPA.

## 1. Introduction

In 21 century REEs have received diverse of applications as components in high technology devices, including smartphones, digital cameras, computer hard disks, fluorescent and light-emitting-diodes, flat-screen televisions, etc. (Dushyantha et al., 2020; Jyothi et al., 2020; Pagano et al., 2019). Therefore, European Commission included REEs to the list of most critical mineral raw materials that are an essential part of both high-tech products and every-day consumer products. According to the latest report, 95% of REEs are produced in China with only 3–8% of end-of-life recycling input rate (European Commission, 2017). Due to a recent high-tech boom with extensive utilization of REE, the amount of REE-containing electronic waste (e-waste) products is growing every year. Thus, the time when alternative sources of REEs will become an important issue is approaching very quickly (Ambaye et al., 2020; Gaustad et al., 2020; Jyothi et al., 2020; Swain and Mishra, 2019). For example, Brazil annually generates about 1.5 million tons of e-waste (Ottoni et al., 2020). Today there are three major applications of REEs

that represent more than 80% of the rare-earth market: permanent magnets (38%), lamp phosphors (32%) and rechargeable batteries (13%) (Binnemans et al., 2013). Thus, it can be assumed that these wastes are the most promising alternative source of REEs.

The problem of e-waste recycling already attracts considerable attention of scientists and industry and it is expected that in long-term global demand for REEs, environmentally sustainable production process shall substitute or supplement current ore sources (Dutta et al., 2016). Besides the intrinsic value as a secondary source of REEs, potentially reducing the consumption of primary raw materials, geopolitical factors make e-waste recycling even more important (European Commission, 2017). Hydrometallurgical and pyrometallurgical techniques are the two most commonly used in REEs recycling techniques (Omodara et al., 2019). Most common hydrometallurgical techniques include dissolving of e-waste in mineral acids (leaching) with further precipitation, solvent extraction (Gergoric et al., 2017), ion exchange (Chour et al., 2018) or adsorption of the target ions (Ambaye et al., 2020; Pramanik et al., 2020). Since solvent extraction is the only

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technology used in mining production, there is a great desire to adapt it for e-waste processing. Unfortunately, REEs separation based on solvent extraction utilizes a lot of toxic and corrosive organic solvents and generates large amounts of waste. Thus, it is not acceptable for installation in urban sites where e-wastes have been generated. Contrary to solvent extraction, solid-phase extraction (SPE) is much more environmentally friendly and more cost-effective. It also offers high enrichment factor, easy and rapid operation. Thus, a lot of attention was paid to the development of SPE technologies for REEs recycling (C.E.D. Cardoso et al., 2019a, 2019b; Hu et al., 2018; Mosai et al., 2019; Pereo et al., 2018; Pramanik et al., 2020; Swain and Mishra, 2019). The adsorbent plays a key role in SPE-based methodology. The ideal SPE adsorbents are expected to feature with the following characteristics: large specific surface area, high chemical and mechanical stability, fast kinetics of adsorption and desorption, reversible adsorption, high selectivity and recovery rate (Hu et al., 2016). Besides the conventional materials, such as activated carbon and alumina (Celso E. D. Cardoso et al., 2019a, 2019b), a variety of novel materials including ion-imprinted polymers, restricted access materials, and metal-organic frameworks have been employed as the adsorbents for solid-phase extraction of REEs (Hu et al., 2016). Mesoporous silicas with immobilized metal-binding ligands meet the requirements for SPE recovery of REEs (Pinta, 2017; Pyrzynska et al., 2016). The silica gel matrix ensures a large surface area of the adsorbent and its high kinetic characteristics, and the immobilized ligands provide the required selectivity and affinity to REEs. Among a variety of ligands, those that form stable complexes with REE are in focus. For example, silica-based adsorbents with immobilized fragments of polydentate aminocarboxylates (Lerner et al., 2019; Zhang et al., 2016), amino-phosphonates (Olena Artiushenko et al., 2020a, 2020b; Callura et al., 2018; Noack et al., 2016) and hydroxamates (O. Artiushenko et al., 2020a, 2020b) were successfully used for preconcentration of REEs (Iftekhhar et al., 2018). Even though derivatives of 2,6-pyridinedicarboxylic acid (dipicolinic acid, DPA) have widely been used in the chemistry of REEs (see, for example (Barja et al., 2011)), adsorption properties of silica-based material with this immobilized DPA toward REEs have not yet been studied.

Several attempts have been made to immobilized DPA on silica surface. For example, 2,6-pyridinedicarboxylate derivative was attached to mesoporous silica surface by thermal treatment of SBA-15 with  $N^2,N^6$ -bis(2-hydroxyethyl)pyridine-2,6-dicarboxamide (Fig. 1b) (Li et al., 2015). However, this approach leads to the formation of hydrolytically unstable Si-O-C bond (see, for example (Engelhardt, 1979)) and thus cannot be recommended for recovery of REEs from water media. Silica-based adsorbents with DPA fragments were also obtained in sol-gel synthesis by hydrolysis of  $N,N$ -bis(trimethoxysilylpropyl)-2,6-pyridine dicarboxamide (Fig. 1c) (Franville et al., 2001; Verma and Dubey, 2020; Yuan et al., 2015).

In contrast to earlier published approaches, in this research, mesoporous silica-based adsorbent with covalently immobilized fragments of 2,6-pyridinedicarboxylic acid ( $SiO_2$ -DPA) has been obtained by surface assembling. Special attention was paid to the synthetic procedure, which allows one to bind the target ligand bounded with the carrier surface via only one carboxylic group (Fig. 1d).

Information about application of DPA-containing adsorbents for recovery of metal ions is very limited. For example, silica-immobilized DPA has been applied for Hg(II) and some other heavy metal preconcentration (Yuan et al., 2015; Zajtsev et al., 2004). In the only publication where DPA-containing adsorbent has been used for REEs preconcentration, it was reported the application of Amberlite XAD-4 with immobilized 2,6-diacetylpyridine (Fig. 1a) for preconcentration of rare earth elements from seawater (Karadaş et al., 2011). However, the adsorbent demonstrated poor REEs retention and limited pH-range of the adsorbent efficiency. For example, recovery of Nd, Ho, Ce and Sm were five times smaller than La, Lu and Yb and optimal conditions for REEs adsorption were achieved in solution with  $pH > 5.0$  (Yuan et al., 2015). Poor adsorption properties of earlier reported DPA-based adsorbents towards REEs might be related to the fact that DPA fragments on such adsorbents have been attached to the support by means of two carboxylic groups (Fig. 1a-c) that can accentually reduce stability of metal complexes and thus affinity of the immobilized ligand towards REEs (Yuan et al., 2015).

In this research, adsorption properties toward REEs of  $SiO_2$ -DPA obtained by surface assembling approach have been investigated. The recovery of REEs from multielement solution and also in the presence of 22 interfering metal ions has been studied, as well as metal adsorption isotherms, adsorption kinetics and  $SiO_2$ -DPA reusability. The adsorbent was successfully applied for selective recovery of rare earth elements from acidic leaching solution of waste fluorescent lamps.

## 2. Experimental section

### 2.1. Chemicals

Silica gel (pore size 60 Å, 40–63 µm particle size, surface area 460–580  $m^2 g^{-1}$ ), (3-Aminopropyl)triethoxysilane (APTES,  $\geq 98\%$ ), 2,6-pyridinedicarbonyl dichloride ( $\geq 97\%$ ),  $N,N$ -Diisopropylethylamine (DIPEA, 99.5%) were purchased from Merck; toluene (99.9%), ethanol (99.8%); europium(III) chloride hexahydrate ( $\geq 99.9\%$ ), terbium(III) chloride hexahydrate (99.9%); nitric acid (ACS reagent, 70%) and hydrochloric acid (ACS reagent, 37%) were supplied from Merck; ICP metal standard solutions: a) multielement solution of 16 REEs with concentration of each metal 100  $mg L^{-1}$ , b) multi-element standard solution IV (22 metals in 6%  $HNO_3$  with concentration of each metal 1000  $mg L^{-1}$ ), c) Fe(III) and Cu(II) standard solutions with

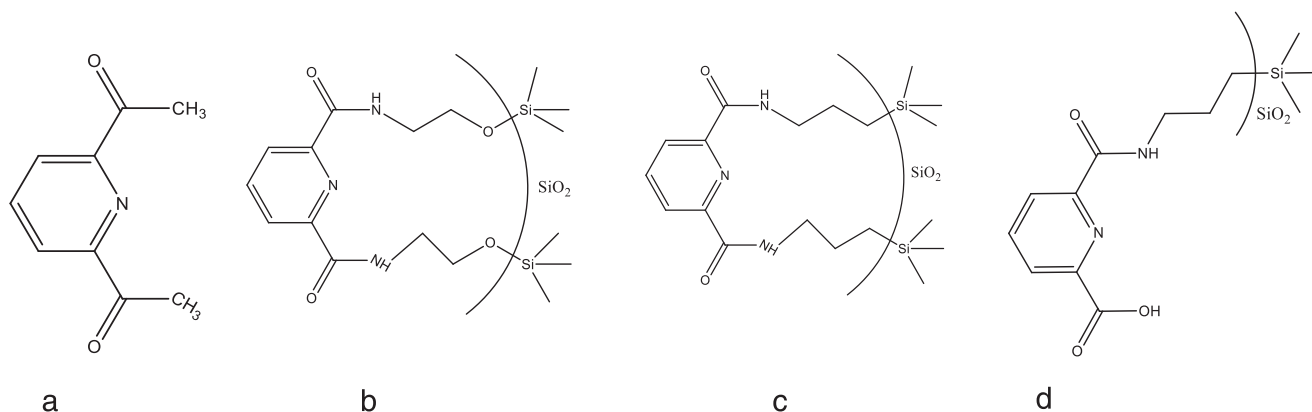


Fig. 1. Schematic illustration of immobilized layer composition on XAD-4 (a), SBA-15 (b), mesoporous silica (c), and currently reported (d) adsorbents, containing 2,6-pyridinedicarboxylic derivatives.

concentration 1000 mg L<sup>-1</sup> - all were obtained from Merck. Toluene was used after drying with calcium hydride. Before modification, silica gel was refluxed in 0.1 mol L<sup>-1</sup> HNO<sub>3</sub> to remove metal impurities and dried in muffle at 550 °C for 6 h. APTES was distilled in a vacuum before utilization. Other chemicals were utilized as received.

The lamp phosphor residue was obtained from an authorized waste repository for discarded lamps at Pontifical Catholic University of Rio de Janeiro, Brazil.

Stock solutions of europium (III) and terbium (III) (1000 mg L<sup>-1</sup>) were prepared by dissolving a weighed quantity of their chlorides in distilled water. The working solutions of desired concentrations were prepared by serial dilution of stock solutions or ICP standards. Ultrapure water obtained from a Milli-Q system was used for the preparation of all types of water solutions.

## 2.2. Syntheses of SiO<sub>2</sub>-DPA

Surface functionalization of silica gel with 2,6-pyridinedicarbonyl dichloride.

At the first stage, silica gel was modified with aminopropyl groups - SiO<sub>2</sub>-(CH<sub>2</sub>)<sub>3</sub>-NH<sub>2</sub> - by treatment with (3-aminopropyl)triethoxysilane in absolute toluene. At the second stage, 0.42 g of 2,6-pyridinedicarbonyl dichloride was mixed with 1.2 mL of N,N-diisopropylethylamine and 100 mL of acetonitrile in a round bottom flask equipped with a mechanical stirrer. Then 1 g of obtained amino silica gel was added under rapid stirring. The reaction was kept under stirring for 4 h at room temperature. Then, the solid phase was separated by filtration, washed with acetonitrile and transferred to a Becker and sodium acetate buffer (pH = 6.0) was added for next 24 h for hydrolysis of anhydride. The resulted adsorbent (SiO<sub>2</sub>-DPA) was separated by filtration, washed in a Soxhlet apparatus with acetonitrile for 24 h and ethanol for further 12 h and dried at 120 °C for 8 h under vacuum. Scheme of SiO<sub>2</sub>-DPA preparation is shown in Fig. 2.

## 2.3. Characterization

FTIR spectra of samples were recorded on FTLA-2000 spectrometer. Textural properties were analyzed using low-temperature nitrogen adsorption-desorption (Micrometrics ASAP 2020). The total pore volume, V<sub>p</sub>, was determined at the maximal adsorption (p/p<sub>0</sub> ≈ 0.99). As for the specific surface area, S<sub>BET</sub>, this parameter was evaluated via standard BET method. The pore size distribution (dV/dx, PSD<sub>V</sub>) and average pore radius (R<sub>ave</sub>) were estimated through two approaches for cylindrical pores - modified Nguyen-Do (MND) (Gun'ko, 2014) and equilibrium model of nonlocal DFT (NLDF) (Landers et al., 2013). CHN elemental analyses were performed on PE-2400 (Perkin Elmer). Thermogravimetric analyses were made on a Pyris 1 TGA (Perkin Elmer). The surface composition was studied by X-ray photoelectron spectroscopy (XPS) using a K-Alpha X-ray photoelectron spectrometer (Thermo Scientific). The surface morphology of neat and modified silica gel particles was

observed with scanning electron microscopy, SEM (JEOL JSM 6490 LV). Luminescent properties of functionalized materials were studied using TGM (Toroidal Grating Monochromator) beamline with an energy range of 3–330 eV (400–4 nm) in Brazilian Synchrotron Light Laboratory. The concentrations of metal ions were determined by inductively coupled plasma mass spectrometry (ICP-MS) model Nexlon 300X, and inductively coupled plasma optical emission spectrometry (ICP-OES) model Optima 7300 DV, both from Perkin Elmer.

## 2.4. Adsorption studies

The adsorption and desorption experiments were performed in a dispersive SPE mode. For this, 10 mg of the adsorbent samples were dispersed in 10 mL of working solution, prepared from ICP standard solution of REEs. The working solution of competitive ions was also added for some experiments at the desired concentrations. The suspension pH was adjusted using 0.1–1.0 mol L<sup>-1</sup> HNO<sub>3</sub>, and then, they were shaken for 0.5–30 min in the falcon tubes. After adsorption equilibrium has been reached, the acidity of the suspensions was measured by pH-meter, 5 mL of the solutions were filtered through a 0.45 μm membrane and analyzed by inductively coupled plasma mass spectrometry (ICP-MS) or inductively coupled plasma atomic emission spectroscopy (ICP-OES). Adsorption of metals (A, %) was determined from five parallel experiments and calculated from Eq. (1):

$$A, \% = \frac{(C_i - C_e) \times 100}{C_i} \quad (1)$$

where C<sub>i</sub>, C<sub>e</sub> – initial and equilibrium concentration of metal ion solution in the aqueous phase, in μg L<sup>-1</sup>.

Desorption experiments were realized using metal-containing samples of SiO<sub>2</sub>-DPA obtained after the adsorption experiments. To do this, each sample was initially rinsed with distilled water with pH= 3.0 and then 10 mL 2.0 mol L<sup>-1</sup> HNO<sub>3</sub> solution was added. The suspensions were left in a shaker for 15 min, and then, the concentrations of metals in the supernatant were determined by ICP-MS. The elution degree (E, %) was determined from five parallel experiments and calculated from Eq. (2):

$$E, \% = \frac{C_e \times 100}{C_i} \quad (2)$$

The overall recovery of the REEs from solution on SiO<sub>2</sub>-DPA was determined from subsequent adsorption and desorption experiments and calculated from Eq. (2). The adsorbent reusability was determined from ten subsequent adsorption/desorption experiments using the same sample of SiO<sub>2</sub>-DPA. After each cycle, the adsorbent was separated by centrifugation and rinsed with water. The supernatant was analyzed by ICP-MS on metal content. The results of the investigation were presented as a violin plot of metal recovery.

For the investigation of REEs adsorption versus pH, the multielement

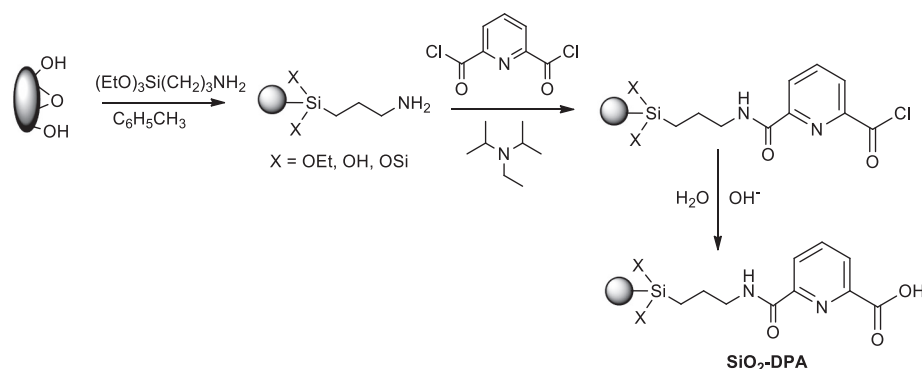


Fig. 2. General scheme of SiO<sub>2</sub>-DPA synthesis by surface assembling.

solution has been used with a concentration of each REE ion - 20.0  $\mu\text{g L}^{-1}$  and concentration of  $\text{Ca}^{2+}$  ion - 1.0  $\text{mg L}^{-1}$  in the pH range 1–7.

The rate of adsorption was studied for  $\text{Eu}^{3+}$  solution with  $\text{pH} = 3.0$  and concentration 10  $\text{mg L}^{-1}$ . Adsorption isotherms were obtained from experiments where samples of  $\text{SiO}_2\text{-DPA}$  (10 mg) were immersed to 10 mL solution of  $\text{Eu}^{3+}$  with  $\text{pH} = 3.0$ . The concentration of Eu in the solutions was varied from 0.1 to 25  $\text{mg L}^{-1}$ . The equilibrium adsorption capacity ( $q_e$ ) and the capacity of the adsorbent at time  $t$  ( $q_t$ ) were calculated from Eq. (3):

$$q = \frac{(C_i - C_e) \times V}{m}, \quad (3)$$

where:  $V$  – volume of the solution (L);  $m$  – adsorbent mass (g).

Distribution coefficients ( $K_d$ ) of REEs between liquid and solid phases were calculated from Eq. (4):

$$K_d = \frac{(C_i - C_e)}{C_e} \times \frac{V}{m}, \quad (4)$$

Interference of foreign ions on REEs recovery has been studied using two types of model solutions. The first type (solution A) contained  $\text{Fe}^{3+}$  and  $\text{Cu}^{2+}$  ions. The second type (solution B) contained 22 metal ions ( $\text{Ag}^+$ ,  $\text{Al}^{3+}$ ,  $\text{Ba}^{2+}$ ,  $\text{Bi}^{3+}$ ,  $\text{Ca}^{2+}$ ,  $\text{Cd}^{2+}$ ,  $\text{Co}^{2+}$ ,  $\text{Cr}^{3+}$ ,  $\text{Cu}^{2+}$ ,  $\text{Fe}^{3+}$ ,  $\text{Ga}^{3+}$ ,  $\text{In}^{3+}$ ,  $\text{K}^+$ ,  $\text{Li}^+$ ,  $\text{Mg}^{2+}$ ,  $\text{Mn}^{2+}$ ,  $\text{Na}^+$ ,  $\text{Ni}^{2+}$ ,  $\text{Pb}^{2+}$ ,  $\text{Sr}^{2+}$ ,  $\text{Tl}^{3+}$  and  $\text{Zn}^{2+}$ ). In the interference experiment, the mass of the adsorbent has kept constant (10 mg) as well as the concentration of each REE (20.0  $\mu\text{g L}^{-1}$  and 100.0  $\mu\text{g L}^{-1}$  for interfering solution A and B, correspondingly), while the concentration of interfered ions was varied from 1 to 32  $\text{mg L}^{-1}$ . The interference effect of 22 metal ions was studied in constant ionic strength created by 0.5  $\text{mol L}^{-1}$  NaCl.

Leaching solution of waste fluorescent lamps has been prepared in the next steps. First, waste fluorescent powder from tubular lamps of different manufacturers was sieved to separate the powder from the glass and dried at 110 °C in vacuum for 2 h using cartridge filled with sulfur powder. Then 0.5 g of waste phosphor powder was treated with 2.5 mL of aqua regia at 80 °C under stirring for 2 h. Finally, the solution was diluted to 10 mL with water and filtered through a 0.45  $\mu\text{m}$  membrane filter. The quantitative analysis of metals in the leaching solution was performed by ICP-MS.

Recovery of REEs from the leaching solution has been studied in dispersive SPE experiment using 5 mL of the diluted leaching solution and 50 mg of  $\text{SiO}_2\text{-DPA}$ . The suspension acidity was adjusted to  $\text{pH} = 3.0$  and a total volume of 25 mL. The suspension has been stirred on a shaker for 30 min and centrifugated. Metal-containing adsorbent was further treated as it is described above for the desorption experiment. The concentration of metal ions has been determined by ICP-MS in the leaching solution, in the supernatant and the concentrate, obtained after REEs desorption.

Relative Enrichment factors (EF) of REEs were determined from Eq. (5).

$$\text{EF} = \frac{(\sum C_M^i)/C_{\text{REEs}}^i}{(\sum C_M^i)/C_{\text{REEs}}^i}, \quad (5)$$

where  $C_M^i$ ,  $C_{\text{REEs}}^i$ ,  $C_M^i$  and  $C_{\text{REEs}}^i$  – concentration of impurities (M) and REEs in the initial solution and the concentrate, correspondingly.

Samples of Eu and Tb-containing  $\text{SiO}_2\text{-DPA}$  were obtained by shaking 100 mg of the adsorbent with 10 mL of europium (III) or terbium (III) working solution (concentration  $2 \cdot 10^{-5}$   $\text{mol L}^{-1}$ ) at  $\text{pH} = 3.0$ . The samples were shaken for about 2 h, then washed with Milli-Q water and dried at 120 °C under vacuum.

Statistical processing of the recovery data was carried out by means of a descriptive analysis summarizing mean values and standard deviations supported with the normality test of dispersion for an overall recovery value.

### 3. Results and discussion

#### 3.1. The adsorbent preparation and quantitative characterization

Immobilization of the target 2,6-pyridinedicarboxylate ligand was performed by surface assembling. In such approach mesoporous silica was firstly modified with 3-aminopropyl-(triethoxysilane) (APTES), then aminosilica ( $\text{SiO}_2\text{-NH}_2$ ) was treated with an excess of pyridine-2,6-dicarbonyl chloride in the presence of hindered amine and finally immobilized carbonyl chloride was hydrolyzed to carboxylic acid, as it is schematically demonstrated in Fig. 2. To increase the yield of the target ligand next procedure was strictly followed:

1. Prior modification mesoporous silica was dried at 500 °C to remove physically and chemically adsorbed water. Under this treatment isolated silanols mainly remain on silica surface;
2. APTES was used freshly distilled to remove partly hydrolyzed oligomers. The solvent used for APTES immobilization was water-free. These precautions reduce the probability of cluster-type topography of surface layer on  $\text{SiO}_2\text{-NH}_2$  and thus high local density of immobilized groups;
3. A large excess of pyridine-2,6-dicarbonyl chloride was used to prevent the formation of arched structures, like those demonstrated in Fig. 1b,c.

The results of CHN analysis of  $\text{SiO}_2\text{-DPA}$  and pristine  $\text{SiO}_2\text{-NH}_2$  are presented in Table S1 together with the calculation procedure used. These results allowed to demonstrate that  $\text{SiO}_2\text{-DPA}$  has 0.36  $\text{mmol g}^{-1}$  of target dipicolinic and about 0.49  $\text{mmol g}^{-1}$  of pristine propylamine fragments, Table 1.

The results of  $\text{SiO}_2\text{-DPA}$  chemical analysis were confirmed by TGA analysis of the adsorbent. The thermogram shows the significant weight loss of  $\text{SiO}_2\text{-DPA}$  at temperature  $> 300$  °C, which corresponds to the thermal decomposition of the organic layer (ESI, Fig. S1). The pristine  $\text{SiO}_2\text{-NH}_2$  also demonstrate weight loss, but significantly less than  $\text{SiO}_2\text{-DPA}$ . From this difference, the concentration of 2,6-pyridinedicarboxylic fragments was estimated as is described elsewhere (Alekseev et al., 2006). The results presented in Table 1 demonstrates good agreement between CHN and thermal analysis.

#### 3.2. Characterization

Nitrogen adsorption/desorption experiment demonstrates that  $\text{SiO}_2\text{-DPA}$  has the  $\text{N}_2$  adsorption/desorption isotherm identical to pristine  $\text{SiO}_2$ . This suggests that immobilization of 2,6-pyridinedicarboxylic fragments does not change the porous structure of silica support having typical Type IV isotherm with a distinct hysteresis loop of H1 within the  $p/p_0$  range of 0.4–1.0, indicating mesopore presence. At high relative pressure, the saturation of the isotherms is clearly observed, and this feature indicates the complete filling of the mesopores and the absence of macropores. The pore size distribution on  $\text{SiO}_2\text{-DPA}$  has a single-mode profile (Fig. 3b). The textural parameters of  $\text{SiO}_2\text{-DPA}$  presented in Table 1 demonstrate that the average pore size of  $\text{SiO}_2\text{-DPA}$  is only slightly less than for the pristine silica. This is an indication that  $\text{SiO}_2\text{-DPA}$

**Table 1**  
Material characterization results.

Material	Porosity Parameters				$C_L^a$ , $\text{mmol g}^{-1}$		
	$S_{\text{BET}}$ , $\text{m}^2 \text{g}^{-1}$	$R_{\text{ave}}$ , nm		$V_p$ , $\text{cm}^3 \text{g}^{-1}$		CHN <sup>b</sup>	TGA
		NLDFT	MND	NLDFT	MND		
$\text{SiO}_2\text{-DPA}$	389	3.5	3.9	0.564	0.581	0.36	0.35

<sup>a</sup>  $C_L$  - loading of functional groups;

<sup>b</sup> calculated from the mass fraction of nitrogen, as it is described in the ESI.

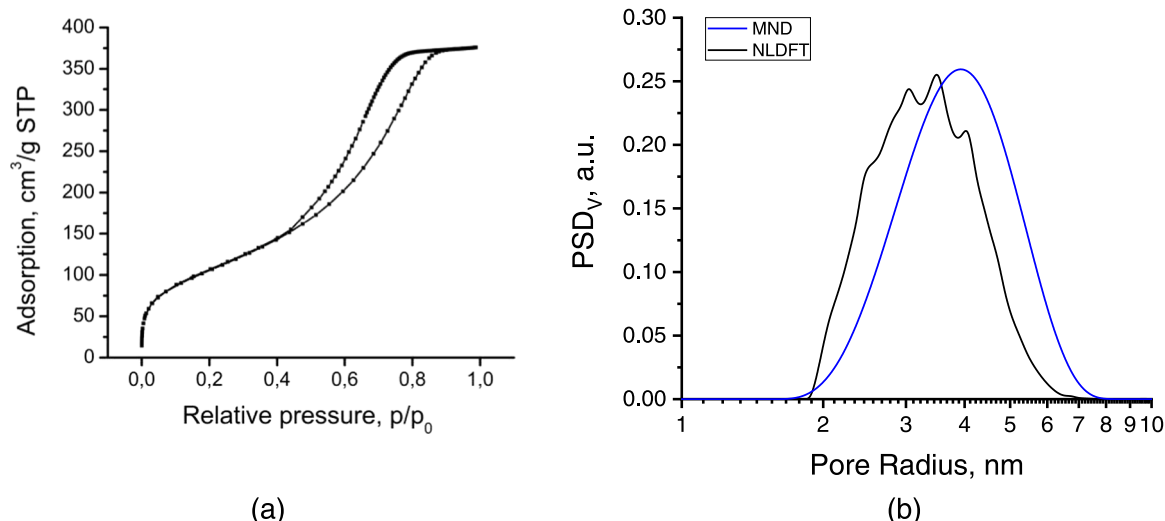


Fig. 3. Isotherm of nitrogen adsorption-desorption (a) and pore size distribution by volume computed with the help of NLDFIT and MND methods (b) for SiO<sub>2</sub>-DPA.

DPA has monolayer of covalently immobilized functional groups obtained by silylation of silica gel surface, rather by the silane hydrolysis (Zaitsev, 2003). This conclusion is indirectly confirmed by CHN analysis of SiO<sub>2</sub>-NH<sub>2</sub> (Table S1).

Scanning electron microscopy images of unmodified silica gel and SiO<sub>2</sub>-DPA demonstrated that the morphology of silica gel was not affected by any changes after manipulations attributed to the immobilization of 2,6-pyridinedicarboxylic acid (Fig. S2).

FTIR spectrum of SiO<sub>2</sub>-DPA demonstrates essential changes in comparison with the spectrum of pristine SiO<sub>2</sub>-NH<sub>2</sub>, Fig. S3. Particularly, in addition to the bands, commonly observed for all silica-based materials, the spectrum of SiO<sub>2</sub>-DPA demonstrates absorbance at 1646, 1546 cm<sup>-1</sup>, that can be attributed to Amide-I and Amide-II bands, resulting from NHC=O stretching and C(O)-NH bending vibrations, correspondingly. Also, narrow peaks at 1420 cm<sup>-1</sup> and 1450 cm<sup>-1</sup> in FTIR of SiO<sub>2</sub>-DPA are respectively attributed to the stretching vibration of C=C and C=N fragments of the pyridine ring. To this point, FTIR spectra confirm the anchoring of pyridine derivatives on aminosilica surface via acylation reaction, Fig. 2.

The survey XPS spectrum of SiO<sub>2</sub>-DPA have bands attributed to the silica matrix elements (Si2p at 103.2 eV, Si2s at 154.3 eV and O1s at 532.5 eV), and immobilized organic fragments (C1s at 284.8 eV and N1s

at 400.5 eV), Fig. 4.

Deconvoluted N1s band in high-resolution XPS of SiO<sub>2</sub>-DPA consists of two components attributed to -NH<sub>2</sub> (399.7 eV) and C(O)-NH (401.9 eV) fragments, while SiO<sub>2</sub>-NH<sub>2</sub> presented only one at 399.7 eV, with a small band at 401.6 eV commonly observed for SiO<sub>2</sub>-NH<sub>2</sub> and attributed to -NH<sub>3</sub><sup>+</sup> groups, Fig. 5.

### 3.3. Adsorption properties of SiO<sub>2</sub>-DPA

#### 3.3.1. Effect of pH

The recovery of metal ions as a function of pH is a crucial parameter that demonstrates affinity of adsorbents to REEs because the pH affects both decompositions of the immobilized complexes and the speciation of metal ions in aqueous media. To eliminate the interference of M(OH)<sub>3</sub> precipitation and their chemisorption, the pH of the hydroxides precipitation was calculated based on solubility product constants ( $K_{sp}$ ) for most common interfering ion ( $M = Fe$ ,  $K_{sp} [Fe(OH)_3] = 6.3 \cdot 10^{-38}$  and one of the target ion ( $M = La$ ,  $K_{sp} [La(OH)_3] = 2.0 \cdot 10^{-21}$ ) ("CRC Handbook of Chemistry and Physics 100th Edition," n.d.). Based on the  $K_{sp}$  calculations, the precipitation pH values for the metal concentration  $10^{-3} \text{ mol L}^{-1}$  were estimated as 2.93 (for Fe(OH)<sub>3</sub>) and 7.2 (for La(OH)<sub>3</sub>), Fig. 6. At pH above these values, the metal hydroxide precipitation is accompanied by the ion chemisorption. Taking into account that

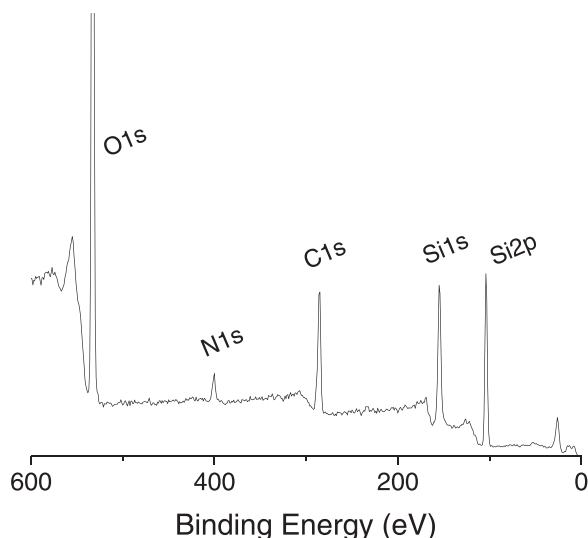


Fig. 4. Survey XPS general spectra of SiO<sub>2</sub>-DPA.

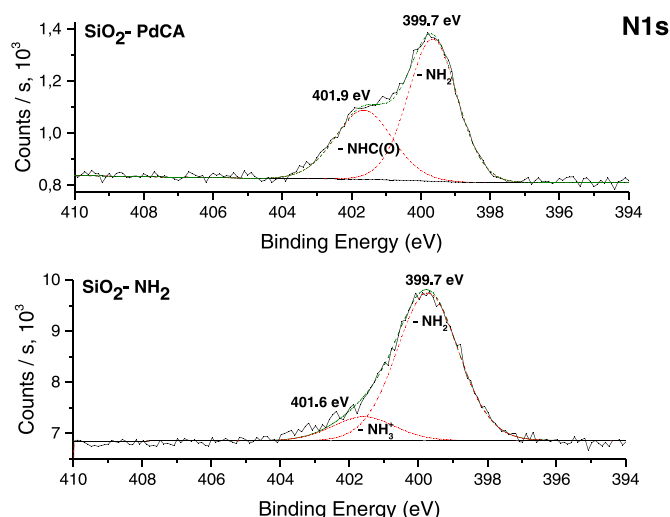
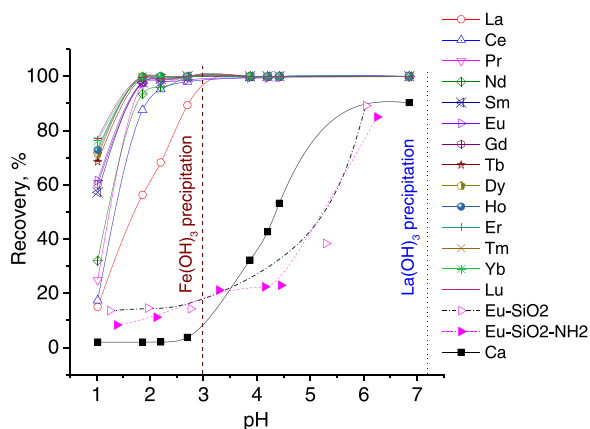


Fig. 5. XPS N1s spectra of SiO<sub>2</sub>-DPA in comparison with SiO<sub>2</sub>-NH<sub>2</sub>.



**Fig. 6.** Effect of pH on adsorption of 13 REEs ions on SiO<sub>2</sub>-DPA, SiO<sub>2</sub> and SiO<sub>2</sub>-NH<sub>2</sub>. Experimental conditions: the adsorbent weight 50 mg, each REE concentration 20.0 μg L<sup>-1</sup>, Ca concentration 1.00 mg L<sup>-1</sup>, suspension volume 10 mL, contact time 30 min.

REEs precipitation is observed at pH > 7.2, the chemisorption properties of SiO<sub>2</sub>-DPA were investigated in the pH range 1.0–7.0, Fig. 6.

To study the specificity of REEs chemisorption on SiO<sub>2</sub>-DPA a set of preliminary experiments were conducted to investigate their adsorption on silica gel and SiO<sub>2</sub>-NH<sub>2</sub>. As shown in Fig. 6, in the pH range from 1.0 to 5.5 adsorption of Eu (III), which was selected for demonstration purposes, on SiO<sub>2</sub> and SiO<sub>2</sub>-NH<sub>2</sub> is essentially less than on SiO<sub>2</sub>-DPA. SiO<sub>2</sub> and SiO<sub>2</sub>-NH<sub>2</sub> also demonstrate the same low adsorption affinity towards other REEs, Fig. S4. In contrary, SiO<sub>2</sub>-DPA has excellent adsorption properties and quantitatively recover nearly all REEs ions from acidic solution within pH > 1.7, Fig. 6. It is important that SiO<sub>2</sub>-DPA adsorbs REEs at pH smaller than pH of Fe(OH)<sub>3</sub> and Al(OH)<sub>3</sub> precipitation, which allows more effective separation of REEs from such abandoned ions as Fe(III) and Al(III). Another most common macro component of REE-containing minerals and e-waste is Ca. Fig. 6 demonstrates that adsorption of Ca ions on SiO<sub>2</sub>-DPA in the pH range 1–3 is negligible.

An essential difference in adsorption properties of SiO<sub>2</sub>-DPA towards REEs and Ca ions, as well as the low affinity of pristine SiO<sub>2</sub>-NH<sub>2</sub> to REEs, confirm chemisorption of REEs on SiO<sub>2</sub>-DPA due to their binding with immobilized 2,6-pyridinecarboxylate fragments. Further evidence of the formation of metal complexes on the adsorbent surface was obtained from investigation of photoluminescent properties of SiO<sub>2</sub>-DPA samples treated by Eu and Tb salts and will be discussed later.

### 3.3.2. Effect of contact time on metal adsorption

The rate of metal adsorption has been studied for solution of Eu<sup>3+</sup> with pH = 3.0 and initial concentration of metal 10 mg L<sup>-1</sup>. Because SiO<sub>2</sub>-DPA has open mesoporous structure and metal-binding sites are situated on the carrier surface, the metal adsorption on it is very fast, and almost finished in 5 min, Fig. 7.

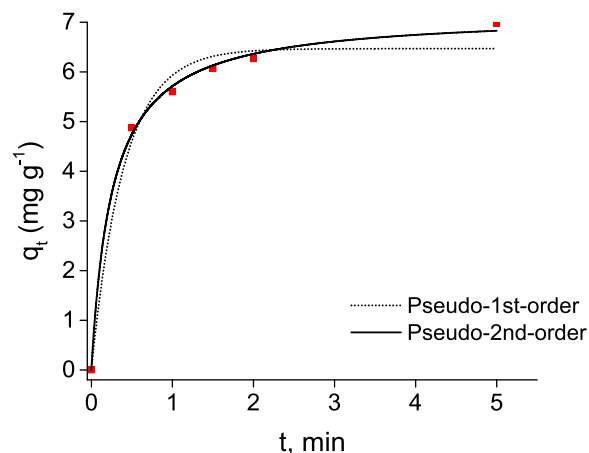
The adsorption data were analyzed by pseudo-1st-order (6) and pseudo-2nd-order (7) models described by equations:

$$q_t = q_e(1 - e^{-k_1 t}), \quad (6)$$

$$q_t = \frac{k_2 q_e^2 t}{1 + k_2 q_e t}, \quad (7)$$

where  $t$  – time, min;  $q_e$  and  $q_t$  – adsorption capacity of metal ions at equilibrium and at time  $t$  (mg g<sup>-1</sup>),  $k_1$  – the rate constant of the pseudo-1st-order model (min<sup>-1</sup>),  $k_2$  – the rate constant of the pseudo-second-order model (g mg<sup>-1</sup> min<sup>-1</sup>).

The calculated kinetic parameters presented in Table 2 demonstrate that pseudo-second-order model better correlates with experimental



**Fig. 7.** The effect of the contact time on Eu<sup>3+</sup> adsorption. Experimental conditions: adsorbent weight - 10 mg, initial metal concentration - 10.0 mg L<sup>-1</sup>, suspension volume - 10 mL, pH 3.0.

**Table 2**

Kinetic parameters for Eu<sup>3+</sup> adsorption.

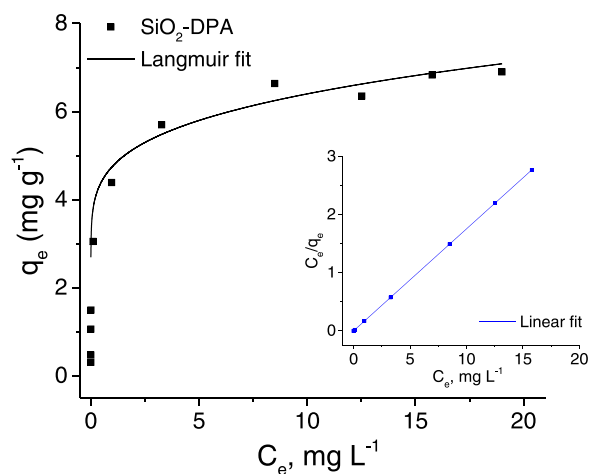
Adsorbent	Pseudo-1st-order			Pseudo-2nd-order		
	$q_e$ , mg g <sup>-1</sup>	$k_1$ , min <sup>-1</sup>	R <sup>2</sup>	$q_e$ , mg g <sup>-1</sup>	$k_2$ , g mg <sup>-1</sup> min <sup>-1</sup>	R <sup>2</sup>
SiO <sub>2</sub> -DPA	6.47	2.49	0.979	7.18	0.543	0.997

data of Eu adsorption on SiO<sub>2</sub>-DPA and thus metal ion diffusion into porous structure of the adsorbent does not limit the adsorption process.

Also, from kinetic parameters, it can be seen that adsorption of REEs on SiO<sub>2</sub>-DPA is reached in minutes, while for chelating resins it can last for hours. These observations support the conclusion made above on monolayered immobilization of chelating groups on mesoporous surface silica and make silica-based adsorbent attractive for REE recovery.

### 3.3.3. Adsorption isotherms

Adsorption isotherm of Eu (III) on SiO<sub>2</sub>-DPA was obtained for the metal solution with pH = 3.0. According to the results presented in Fig. 8, it can be attributed to H-type isotherm, suggesting strong chemisorption of REEs on SiO<sub>2</sub>-DPA with quantitatively recover of Eu (III) from the solution.



**Fig. 8.** Eu (III) adsorption isotherm on SiO<sub>2</sub>-DPA and Langmuir linear fit (inset). Experimental conditions: adsorbent weight - 10 mg, metal concentration range - 0.1–25 mg L<sup>-1</sup>, suspension volume - 10 mL, pH 3.0, contact time - 30 min.

The adsorption data were fitted on the basis of the Langmuir and Freundlich isotherm models. The linearized form of the Langmuir (8) or Freundlich (9) isotherm equations can be represented as:

$$\frac{1}{q_e} = \frac{1}{q} + \frac{1}{C_e} \frac{1}{qK_L} \quad (8)$$

$$\ln q_e = \ln K_F + \frac{\ln C_e}{n} \quad (9)$$

where  $q_e$  - the amount of solute adsorbed ( $\text{mg g}^{-1}$ ),  $C_e$  - equilibrium ion concentration in the solution ( $\text{mg L}^{-1}$ ),  $q$  - saturated adsorption capacity ( $\text{mg g}^{-1}$ ) and  $K_L$  - Langmuir adsorption constant ( $\text{L mg}^{-1}$ ).  $n$  - Freundlich constant and  $K_F$  - binding energy constant reflecting the affinity of the adsorbents to metal ions ( $\text{mg g}^{-1}$ ).

The adsorption behavior of  $\text{Eu}^{3+}$  on  $\text{SiO}_2\text{-DPA}$  has been better fitted by the Langmuir model, Table 3. This indicates the formation of a monolayer of the adsorbate, which correlates with a model of REEs chemisorption due to formation of metal complexes with immobilized 2,6-pyridinedicarboxylate derivatives.

### 3.3.4. The affinity of $\text{SiO}_2\text{-DPA}$

To investigate affinity of  $\text{SiO}_2\text{-DPA}$  toward REEs, metal distribution coefficients ( $K_d$ ) were calculated for Henry region of the adsorption isotherms, using Eq. 3. The metal adsorption experiment was performed for multielement solution of REEs with pH 3.0 and the results were compared with similar experiments performed for  $\text{SiO}_2\text{-NH}_2$  and  $\text{SiO}_2$ . The results presented in Fig. 9 demonstrate that  $K_d$  values for metal adsorption on  $\text{SiO}_2\text{-DPA}$  are in 10–15 times higher than on pristine silicas and reach values  $10^4 \text{ mL g}^{-1}$ . This observation demonstrates a high potential of  $\text{SiO}_2\text{-DPA}$  for quantitative recovery of REEs from acidic water solutions.

### 3.3.5. Adsorption and desorption cycles

Adsorption properties of  $\text{SiO}_2\text{-DPA}$  have been studied for the multielement solution of 14 REEs with pH = 3.0 at the conditions when essential excess of the binding sites is provided (Henry region of the adsorption isotherm). These conditions were selected to prevent non-specific co-precipitation of easy-hydrolyzed ions, such as Al(III) and Fe (III) at the higher pH, Fig. 6. Also, being strong chelating ligand, immobilized 2,6-pyridinedicarboxylate fragments can react with transition and post-transition metal ions (Fig. S5) which can result in the reduction of  $\text{SiO}_2\text{-DPA}$  capacity toward target REEs (Macauley and Hong, 1995; Zajtsev et al., 2004). The results of the investigation presented in Fig. 10a demonstrate that  $\text{SiO}_2\text{-DPA}$  quantitatively adsorbs all REEs in the selected conditions. Slight decrease in adsorption was observed for Ce, Pr and Gd ions, which can be explained by the lower stability of their complexes with immobilized ligands (Jernström et al., 2007).

Desorption of REEs from  $\text{SiO}_2\text{-DPA}$  has been investigated using solutions of  $\text{HNO}_3$ , EDTA and oxalic acid, Fig. S6. It was found that  $2 \text{ mol L}^{-1}$  water solution of  $\text{HNO}_3$  demonstrates the best eluting properties, allowing to achieve complete (95–100%) elution of all REEs, Fig. 10b. This solution has been used in all further experiments for REEs desorption.

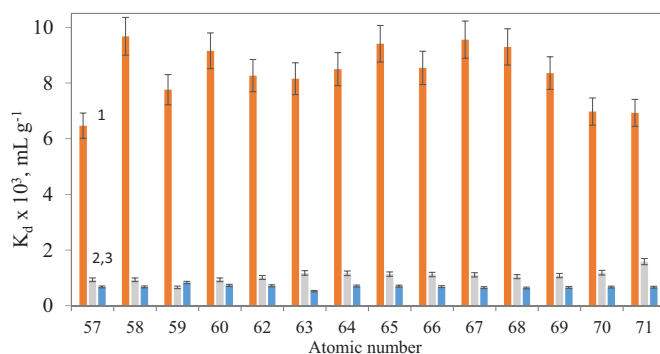
### 3.3.6. The adsorbent reusability

Reusability of the adsorbent has been studied in the course of ten adsorption/desorption cycles by evaluation of overall recovery of REEs.

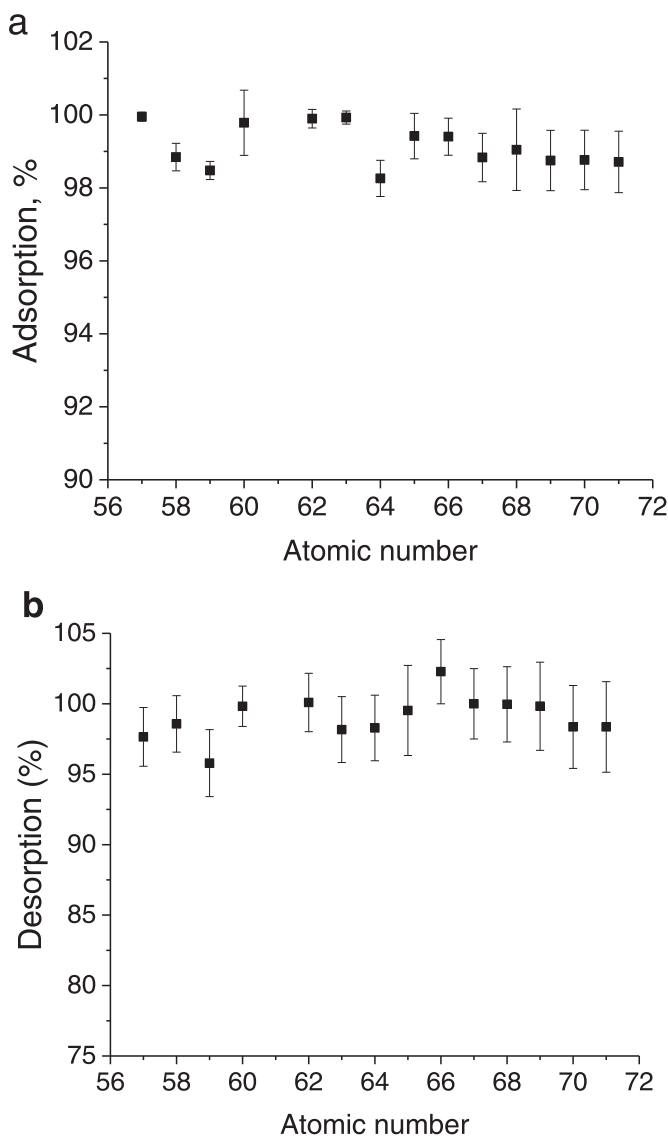
**Table 3**

Adsorption isotherm parameters.

Adsorbent	Langmuir's isotherm model			Freundlich's isotherm model		
	$q_{\text{max}}, \text{mg g}^{-1}$	$K_L, \text{L mg}^{-1}$	$R^2$	$K_F, \text{mg g}^{-1}$	$1/n$	$R^2$
$\text{SiO}_2\text{-DPA}$	5.7	0.361	0.999	3.9	0.270	0.911



**Fig. 9.** Distribution coefficients ( $K_d$ ) of REEs on  $\text{SiO}_2\text{-DPA}$  (1),  $\text{SiO}_2\text{-NH}_2$  (2) and  $\text{SiO}_2$  (3). Experimental conditions: adsorbent weight - 10 mg, initial metal concentration -  $1.0 \text{ mg L}^{-1}$ , suspension volume - 10 mL, pH 3.0, contact time - 30 min.



**Fig. 10.** Adsorption of REEs from multielement water solution in pH = 3.0 on  $\text{SiO}_2\text{-DPA}$  (a) and their desorption by  $2 \text{ mol L}^{-1} \text{ HNO}_3$  (b). Experimental conditions of adsorption: adsorbent weight - 10 mg, REEs concentration -  $100.0 \text{ } \mu\text{g L}^{-1}$  of each metal, suspension volume - 10 mL, contact time - 30 min. The data were obtained from five independent experiments.

The average value with upper and lower limits for all ten cycles is presented in Fig. 11.

From the results presented in Fig. 11, it can be seen that SiO<sub>2</sub>-DPA can be successfully used for REEs recovery for at least in ten consecutive adsorption/desorption cycles with no noticeable loss of the adsorbent efficiency and with a mean value of REEs recovery larger than 97.8% (Table S3). From asymmetric distortion in upper and down parts of the violins it is clear that uncertainty of the recovery degree increases from light to heavy REEs, Fig. 11. It is probably related to incomplete desorption of heavy REEs in each cycle (see Fig. 10). Although the 95% confidence bars are available on the plots (Fig. 11), they demonstrate that a major part of the “violins” typically lies at the probability of 5%.

### 3.3.7. The SiO<sub>2</sub>-DPA selectivity

Recovery of REEs on SiO<sub>2</sub>-DPA was investigated in increased concentration of different foreign ions. Firstly, interference of Fe<sup>3+</sup> and Cu<sup>2+</sup> having a strong affinity to immobilized ligands (see Fig. S5) has been studied. The results presented in Fig. 12 demonstrate that generally speaking, recovery of REEs on SiO<sub>2</sub>-DPA is decreased with increasing Cu and Fe concentration, but this decrease is essential for the recovery of La, Ce, Pr, Nd and Sm ions. For other REEs, even 3200-fold excess of Fe and Cu ions reduces REEs recovery only to 80–86%.

The second interfering solution used for investigation of SiO<sub>2</sub>-DPA selectivity (solution B) was prepared in 0.5 mol L<sup>-1</sup> NaCl and consists of three groups of ions: a) alkaline and alkaline earth metals (Li<sup>+</sup>, Na<sup>+</sup>, K<sup>+</sup>, Mg<sup>2+</sup>, Ca<sup>2+</sup>, Sr<sup>2+</sup> and Ba<sup>2+</sup>); b) transition metal (Cr<sup>3+</sup>, Mn<sup>2+</sup>, Fe<sup>3+</sup>, Co<sup>2+</sup>, Ni<sup>2+</sup>, Cu<sup>2+</sup>, Ag<sup>+</sup>), and c) post-transition metals (Zn<sup>2+</sup>, Cd<sup>2+</sup>, Al<sup>3+</sup>, Ga<sup>3+</sup>, In<sup>3+</sup>, Tl<sup>3+</sup>, Pb<sup>2+</sup> and Bi<sup>3+</sup>). Five samples of solution B with the concentration of each foreign ions from 1 mg L<sup>-1</sup> to 16 mg L<sup>-1</sup> have been added to SiO<sub>2</sub>-DPA, while the concentration of each REE was kept constant (100 μg L<sup>-1</sup>). The total concentration of the only transition and post-transition metal ions in solution B is up to 240 mg L<sup>-1</sup>, which constitutes their 2400-fold excess to REEs ions. Therefore, solution B more essentially reduce REEs recovery than solution A, Fig. 13. Similar to solution A, recovery of light REEs (and particularly La and Ce) from solution B falls up to 8–9%. Nevertheless, the recovery of heavy REEs (from Eu to Lu) declines only on 20–30%, Fig. 13.

These experiments demonstrate the great potential of SiO<sub>2</sub>-DPA to recover REEs even from complex solutions having large excess of transition and post-transition metals and high concentration (at least 30 g L<sup>-1</sup>) of NaCl.

High selectivity noticed for SiO<sub>2</sub>-DPA can be explained by complexation of immobilized derivatives of 2,6-pyridinecarboxylic acid with REEs. This statement is supported by the results obtained from the investigation of photoluminescent properties of SiO<sub>2</sub>-DPA treated by Eu

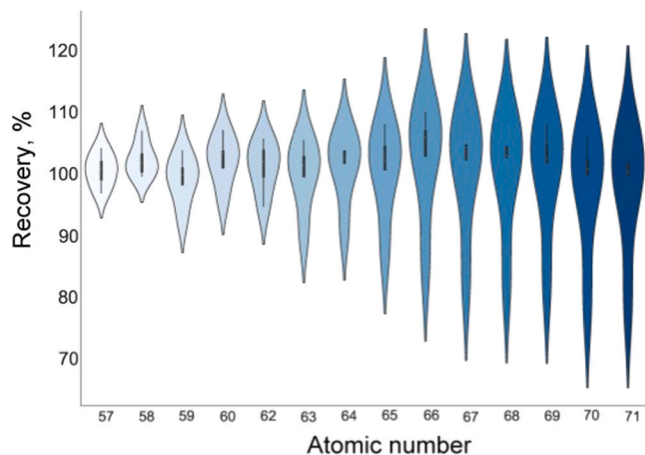


Fig. 11. The violin plots on the recovery of REEs on SiO<sub>2</sub>-DPA from multielement water solution in pH= 3.0 with further desorption by 2 mol L<sup>-1</sup> HNO<sub>3</sub> in ten adsorption-desorption cycles.

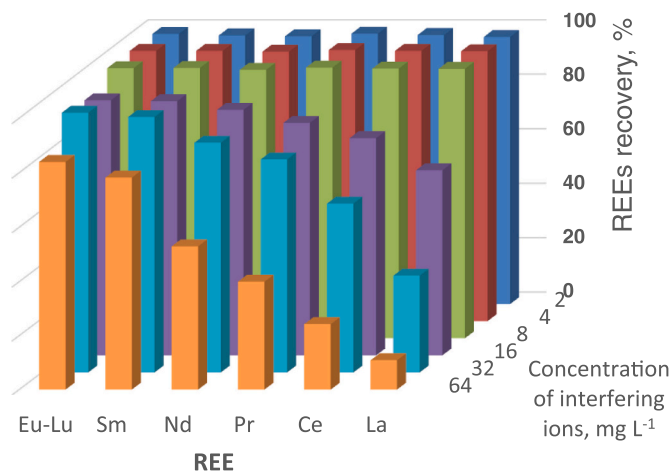


Fig. 12. Recovery of REEs by SiO<sub>2</sub>-DPA from solutions containing different concentration (from 1 to 64 mg L<sup>-1</sup>) on interfering ions (Fe and Cu).

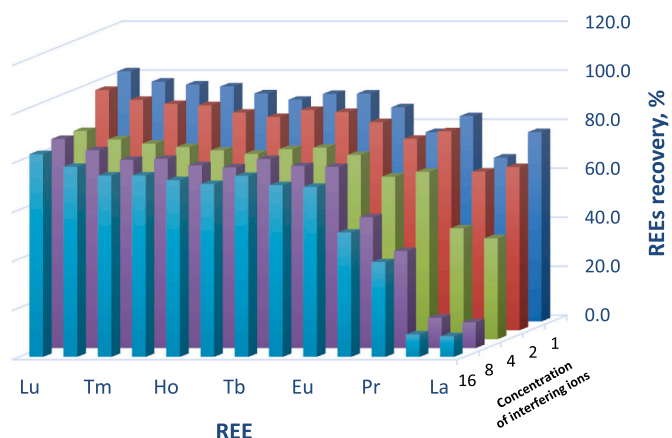


Fig. 13. Recovery of REEs by SiO<sub>2</sub>-DPA from solutions containing different concentration (from 1 to 16 mg L<sup>-1</sup>) on interfering ions of the solution B.

and Tb ions.

### 3.4. Photoluminescent properties of immobilized Eu and Tb complex

It is known that Eu and Tb ions form stable complexes with 2,6-pyridinedicarboxylic acid, which demonstrate strong red (Eu) and green (Tb) photoluminescence (PL) (Maji et al., 2015). To prove that adsorption of REEs from water solution is observed due to their complexation with immobilized ligands, PL spectra of Tb<sup>3+</sup> and Eu<sup>3+</sup> containing samples of SiO<sub>2</sub>-DPA were investigated. For this, the adsorbent was immersed into a water solution of corresponding salts with pH = 3.0 and, after 15 min of contact, the precipitate was separated by decantation, washed with water several times and dried in vacuum at room temperature. It was found that resulted in solids emit visible by necked eye red (for Eu) and green (for Tb) light under illumination with UV-lamp, Fig. 14.

The 3D PL emission spectra of Eu and Tb-containing SiO<sub>2</sub>-DPA excited within the 4–6 eV energy at room temperature confirm that photoluminescence of the solids is due to electron transitions in f-elements. Fig. 14.

Indeed, after adsorption of Eu<sup>3+</sup> or Tb<sup>3+</sup> ions, silica composites demonstrate strong luminescent emissions between 480 and 650 nm, that can be attributed to 4f → 4f transitions of the <sup>5</sup>D<sub>0</sub> excited state to the low-lying <sup>7</sup>F<sub>J</sub> (J = 0, 1, 2, 3, 4) levels of Eu<sup>3+</sup> ions and <sup>5</sup>D<sub>4</sub> → <sup>7</sup>F<sub>n</sub> (n = 3, 4, 5, 6) electron transitions of the Tb<sup>3+</sup> ions. No emission peaks

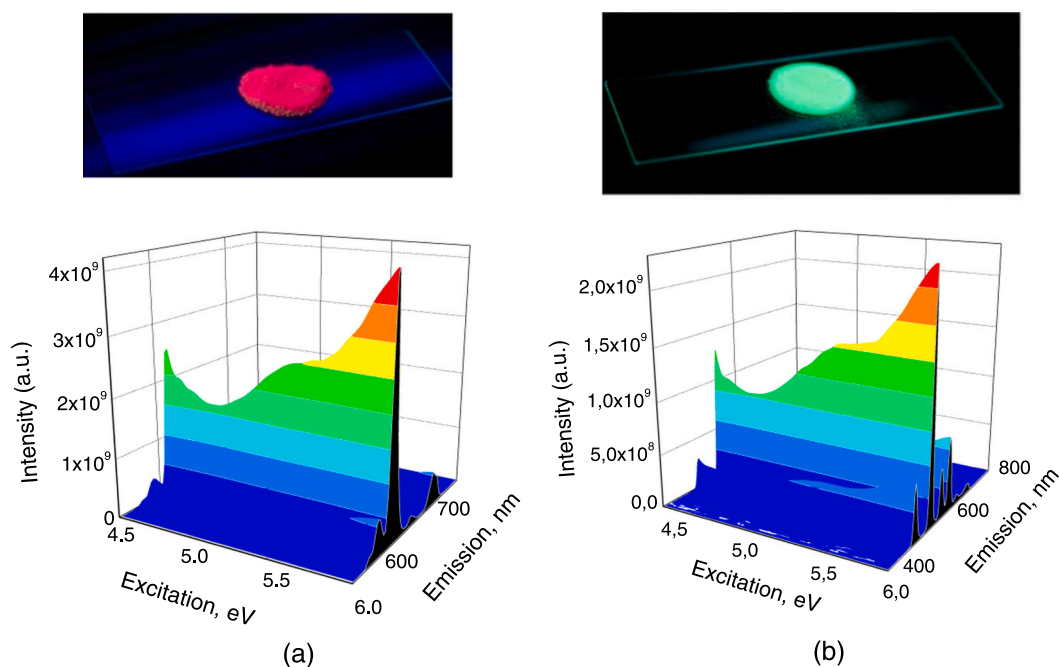


Fig. 14. Photo and 3D mapping of PL spectra for of SiO<sub>2</sub>-DPA samples treated by Eu (a) and Tb (b) ions.

from the ligands were observed under this excitation.

Example of 2D emission spectra of Eu and Tb containing SiO<sub>2</sub>-DPA are shown in Fig. 15.

Regardless that spectra were recorded for solid samples at room temperature, they demonstrate well-separated emission peaks, which allowed to determine the composition and geometry of immobilized metal species. For example, PL spectrum of SiO<sub>2</sub>-DPA-Eu is very similar to individual Eu complex with 2,6-pyridinedicarboxylate (DPA), Na[Eu(DPA)<sub>3</sub>] (Murray et al., 1990). Particularly, PL spectrum of SiO<sub>2</sub>-DPA-Eu has no peak for forbidden <sup>5</sup>D<sub>0</sub> → <sup>7</sup>F<sub>0</sub> transitions, peak attributed to <sup>5</sup>D<sub>0</sub> → <sup>7</sup>F<sub>3</sub> forbidden transition at 650 nm is very weak, <sup>5</sup>D<sub>0</sub> → <sup>7</sup>F<sub>1</sub> and <sup>5</sup>D<sub>0</sub> → <sup>7</sup>F<sub>4</sub> transitions can be deconvoluted into two peaks each, while <sup>5</sup>D<sub>0</sub> → <sup>7</sup>F<sub>2</sub> is the strongest one and has only one component, Fig. 15. The presence of <sup>5</sup>D<sub>0</sub> → <sup>7</sup>F<sub>2</sub> transitions of Eu<sup>3+</sup> and <sup>5</sup>D<sub>4</sub> → <sup>7</sup>F<sub>5</sub> of Tb<sup>3+</sup> reveals that metal adsorption on SiO<sub>2</sub>-DPA takes place due to the formation of the metal complexes with immobilized derivatives of 2,6-pyridinedicarboxylic acid, as it is schematically demonstrated in Fig. 16.

### 3.5. Recovery of REEs from leaching solution of waste fluorescent lamps

SiO<sub>2</sub>-DPA was applied for the recovery of REEs from the waste of fluorescent lamps. The waste fluorescent powder was collected from tubular lamps of various types and manufacturers. After adjustment of pH, the adsorbent was immersed to the leaching solution, then separated by centrifugation and rinsed and, finally, the eluting solution was added. The concentration of metals was determined in the leaching and eluting solutions, as well as in supernatant. According to the multielement analysis of the leaching solution (Table S2) it consists of alkaline, alkaline earth, transition and post-transition metals, and particularly: Ca (84%), Na (5%), Al (5%), Mn (1.54%), Sb (1.73%) and only 0.02% of REEs, Fig. 17a. Application of SiO<sub>2</sub>-DPA allowed essential changes in the composition of the target solution. First of all, its total salinity drops down to 0.07 g L<sup>-1</sup> (4.6 g L<sup>-1</sup> for leaching solution). The concentration of alkaline earth ions decreased 4000–200 times; Mn and Al 500 times, Fe and Sb 100–57 times, while losses of REEs in the leaching solution were less than 17%, Table S2. The leaching solution mainly consists of Na (29%), Zn (21%), Sb (12%) and REEs (12%), Fig. 17b. Application of

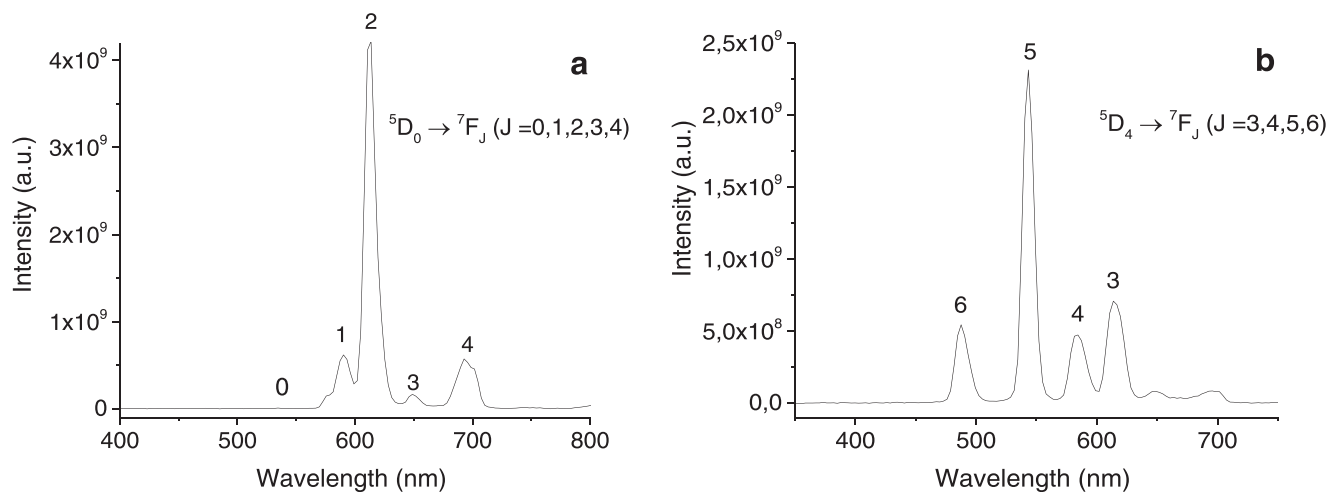


Fig. 15. PL spectra of SiO<sub>2</sub>-DPA-Eu (a) and SiO<sub>2</sub>-DPA-Tb (b).

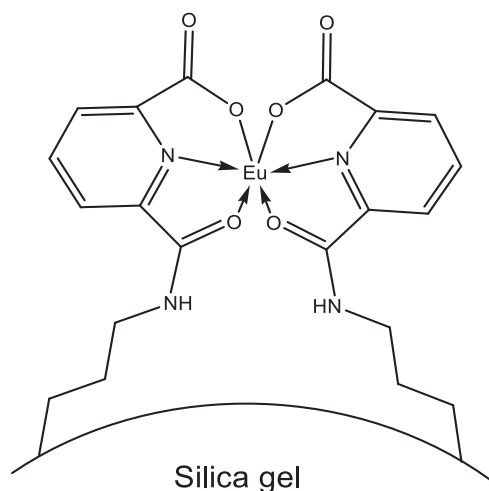


Fig. 16. Schematic structure of Eu complexes with fragments of immobilized 2,6-pyridinedicarboxylic acid.

SiO<sub>2</sub>-DPA allowed to recover 83% of REEs from acidic leaching solution of fluorescent lamp waste, with enrichment factor ER= 615.

From the concise results of REEs determination shown in Table 4, it can be seen that recovery of almost all REEs is above 80%, only the

recovery of La decreases to 50%, similarly to results obtained for model solutions (see Fig. 13).

It is important to mention that, regardless of the essential difference in composition of leaching and eluting solutions, distribution of the recovered REEs is almost identical to its initial distribution in the leaching solution, Fig. 18. This fact confirms the appropriateness of the sample preparation procedure and precisions of the analysis.

#### 4. Conclusions

Mesoporous silica functionalized with fragments of dipicolinic acid was shown to be highly effective in adsorbing lanthanides from the synthetic solution containing a large excess of transition and post-transition ions and from real leaching solution from the waste of fluorescent lamps. SiO<sub>2</sub>-DPA is capable for quantitative adsorption of REE from acidic solution with pH > 1.7, while adsorption of transition metals is observed at lower acidity. Due to this effect adsorption of macro-components of the leaching solution such as Na, Ca, Mg, Ba, Sr, Mn, Al and Sb has no or little influence on REEs recovery. Thus SiO<sub>2</sub>-DPA can be used for recycling of REE from e-waste. Complete elution of adsorbed REE was achieved with 2.0 mol L<sup>-1</sup> HNO<sub>3</sub>, with no degradation in adsorbent performance over multiple reuse cycles.

#### CRediT authorship contribution statement

Olena Artiushenko: Methodology, Investigation, Writing - original

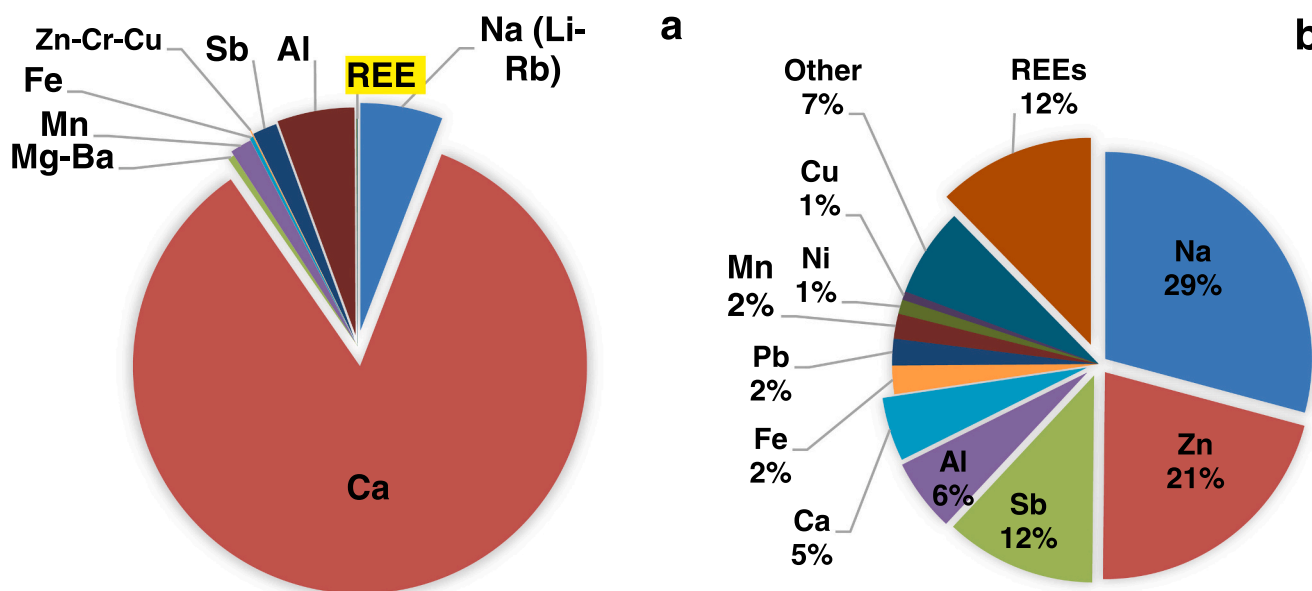


Fig. 17. Distribution of metal ions in the leaching (a) and the eluting (b) solutions.

Table 4

The results of REEs determination in the leaching solution obtained from waste fluorescent lamps.

REE	determined in the leaching solution, mg L <sup>-1</sup>	determined in the supernatant mg L <sup>-1</sup>	degree of adsorption, %	determined in the eluting solution, mg L <sup>-1</sup>	Recovery, %
Y	0.39	<0.01	>96	0.33	80
Eu	0.17	<0.005	>96	0.15	85
Tb	0.15	<0.003	>98	0.12	79
Yb	0.12	<0.002	>98	0.085	67
La	0.014	<0.005	>67	0.011	52
Gd	0.077	<0.002	>98	0.067	85
Sm	0.051	<0.002	>97	0.046	87
Nd, Ce, Er	<0.030	<0.002	100–92	0.03–0.025	68–93
Dy, Pr, Ho, Tm, Lu	<0.005	<LOD	100	0.005–0.002	83–90
REEs total	1.069			0.887	83%

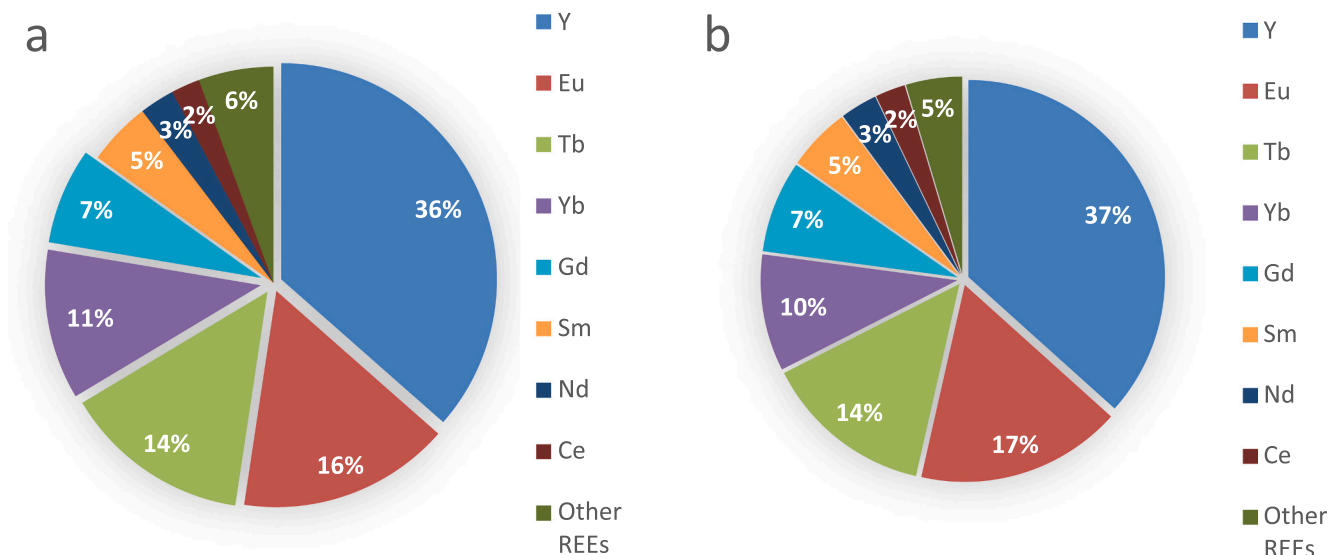


Fig. 18. Distribution of REEs ions in the leaching (a) and the eluting (b) solutions.

draft. **Vladimir Zaitsev**: Conceptualization, Supervision, Writing - original draft, Writing - review & editing. **Wendy S. Rojano**: Investigation. **Gabriel A. Freitas**: Investigation. **Michael Nazarkovsky**: Software, Visualization, Writing - review & editing. **Tatiana D. Saint'Pierre**: Data curation, Formal analysis. **Jiang Kai**: Conceptualization, Writing - review & editing.

#### Declaration of Competing Interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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#### Appendix A. Supporting information

Supplementary data associated with this article can be found in the online version at [doi:10.1016/j.jhazmat.2020.124976](https://doi.org/10.1016/j.jhazmat.2020.124976).

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